

centre de recherche PARIS - ROCQUENCOURT

Flow, transport and chemistry in porous media : numerical methods for coupled problems

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EPFL May 7, 2008

Partially funded by Cnrs GDR MOMAS



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Subsurface flow and transport



Basic models and methods

- Flow model
- Transport model
- Chemistry

Reactive transport

- Single species with sorption (joint work with A. Taakili)
- Multi-species equilibrium chemistry

Motivations

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- Assess safety of deep geological nuclear waste storage (clay layer)
- Long term simulation of radionuclide transport (one million years)
- Wide variation of scales : from package (meter) to regional (kilometers)
- Geochemistry: large number of species
- Strong government regulation



 Research in mathematical and numerical modeling is conducted in the CNRS MOMAS group (Director A. Ern).

Main actors :

Present choice in France: a sedimentary geological formation (in the Meuse region)





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Used as a benchmark, similar to Andra safety model



Blown-up 30 times vertically

Difficulties

- Distorted geometry (horizontal \approx 40 km, vertical 700 m)
- Strong heterogenities (permeability varies by 8 orders of magnitude)
- General hexahedral mesh
- Simulation over 500 000 years



Sleipner project, Norway

- Long term capture of CO₂ in saline aquifer
- Simulation to understand CO₂ migration through salt
- Coupling of liquid and gas phase, reactive transport

SHPCO project (funded by ANR) High Performance Simulation of CO2 sequestration

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Darcy's law and mixed finite element

Flow equations $q = -K\nabla h$ Darcy's lawh piezometric head $\nabla \cdot q = 0$ incompressibilityq Darcy velocity

Mixed finite elements

- Approximate both head and velocity
- Continuous flux across element faces
- Locally mass conservative
- Allows full diffusion tensor



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Subsurface flow and transport

The problem

Standard convergence theory not valid for RTN space over general (deformed) hexahedra, pressure space does not containt constant functions (T. Russell)

Kuznetsov, Repin (2003): construct macroelement on a hexahedron by subdividing it into 5 tetrahedra



Features

- Same DOFs as before (average pressure in each element, flux across each face)
- Standadrd error estimates shown to apply: optimal order error (under regularity assumption).

Construction

$$\mathscr{W}_{h} = \big\{ \mathbf{v}_{h} \in H(\operatorname{div}, \Omega); \, \mathbf{v}_{h|T_{i}} \in RTN_{0}(T_{i}), i = 1, \cdots, 5, \big\}$$

div \mathbf{v}_h const. on H, $\mathbf{v}_h \cdot \mathbf{n}$ constant on faces of H}.

 \mathbf{v}_{hH} is uniquely defined by its normal components across the 6 faces, so \mathcal{W}_h contains constants.

A. Sboui's PhD thesis, Sboui, Jaffr , Roberts to appear in SIAM J. SCi. Comp.

A composite mixed finite element for hexahedra (3)

Simulation for 3D far field benchmark model, horizontal cros section of modulus of velocity



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Convection-diffusion equation



Dispersion tensor

$$\mathbf{D} = d_{e}\mathbf{I} + |\mathbf{u}|[\alpha_{I}\mathbf{E}(\mathbf{u}) + \alpha_{t}(I - \mathbf{E}(\mathbf{u}))], \quad E_{ij}(\mathbf{u}) = \frac{u_{i}u_{j}}{|\mathbf{u}|}$$

 α_l, α_t dispersicity coeff. [m], d_e molecular diffusion [m/s²]

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Advection step

Explicit, finite volumes / discontinuous Galerkin

- Locally mass conservative
- Keeps sharp fronts
- Small numerical diffusion
- Allows unstructured meshes
- CFL condition: use sub-time-steps



Dispersion step

Like flow equation (time dependant): mixed finite elements (implicit)

First order method

Example: transport around an obstacle

MoMaS benchmark for reactive transport. Here transport only



Head and velocity

Concentration at t = 25



J. B. Apoung, P. Hav, J. Houot, MK, A. Semin, O. Saouli

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Transport around a nuclear waste storage site

GdR MoMaS benchmark, Andra model





Concentration at 130 000 years

Concentration at 460 000 years

A. Sboui, E. Marchand (INRIA, Estime)

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Chemical phenomena



Subsurface flow and transport

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According to nature of reaction

Homogeneous In the same phase (aqueous, gaseous, ...) Examples: Acid base, oxydo-reduction

Heterogeneous Involve different phases

Examples: Sorption, precipitation / dissolution, ...



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According to speed of reaction

Slow reactions Irreversible, modeled using kinetic law

Fast reactions Reversible, modeled using equilibrium

Depends on relative speed of reactions and transport.

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In this talk: Equilibrium reactions, with sorption.



Definition

Sorption is the accumulation of a fluid on a solid at the fluid–solid interface.

Main mechanism for exchanges between dissolved species and solid surfaces.



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Several possible mechanisms

Surface complexation Formation of bond between surface and aqueous species, due to electrostatic interactions. Depends on surface potential.

Ion exchange Ions are exchanged between sorption sites on the surface. Depends on Cationic Exchange Capacity.

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Can be modeled as mass action law



Modeling general equilibrium models

General chemical reactions : N_s species, N_r reactions

$$\sum_{j=1}^{N_s} v_{ij} \mathbf{Y}_j \leftrightarrows \mathbf{0}, \quad i = 1, \dots, N_r$$

 v_{ii} stoichiometric coefficients. Matrix equation v Y = 0



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v has full rank : Rank $v = N_r$.

Basis for null-space of v has dimensions $N_c = N_s - N_r$.



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Partition $v = (G \ N)$, $B \in \mathbf{R}^{N_r \times N_r}$ invertible, $N \in \mathbf{R}^{N_c \times N_r}$. Let $H = -G^{-1}N$ General solution of v Y = 0: $Y = \begin{pmatrix} x \\ c \end{pmatrix}$, x = Hc. $c \in \mathbf{R}^{N_c}$, $x \in \mathbf{R}^{N_r}$.

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The chemical problem

c (resp \overline{c}) mobile (resp. fixed) primary species *x* (resp \overline{x}) mobile (resp. fixed) secondary species

System of non-linear equations

$$\begin{array}{c} c + S^{T} x + A^{T} \overline{x} = T, \\ \overline{c} + B^{T} \overline{x} = W, \end{array} \right\} \quad \text{Mass conservation} \\ \log x = S \log c + \log K, \\ \log \overline{x} = A \log c + B \log \overline{c} + \log \overline{K}. \end{array} \right\} \quad \text{Mass action law}$$

Role of chemical model

Given T (and W, known), split into mobile C and fixed F concentrations.

$$C = c + S^T x = \Phi(T), \qquad F = A^T \overline{x} = \Psi(T)$$

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Sorption models

One species reacts with rock matrix, description by a sorption isotherm : $v = \Psi(u)$.

u aqueous concentration, v fixed "concentration"

Common isotherms

Linear
$$\mathbf{v} = K_d \mathbf{u}$$

Langmuir $\mathbf{v} = \frac{k_f \sigma_0 \mathbf{u}}{k_f \mathbf{u} + k_b}$
Freundlich $\mathbf{v} = \gamma \mathbf{u}^{1/p}$ ($p > 1$ possible)

Coupled model

$$\omega \frac{\partial u}{\partial t} + \omega \frac{\partial v}{\partial t} + Lu = 0, \quad L \text{ adv. diff operator}$$
$$v = \Psi(u).$$

Mathematical, numerical analysis: van Duijn, Knabner, Barrett, Kacur, Frolkovic

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After space and time discretization,

Coupled formulation F(u, v) = 0 with

$$F\begin{pmatrix} u\\ v \end{pmatrix} = \begin{pmatrix} (M+\Delta L)u + Mv + b\\ v - \Psi(u) \end{pmatrix}$$

Eliminate \mathbf{v} $F_1(\mathbf{u}) = (M + \Delta tL)\mathbf{u} + M\Psi(\mathbf{u}) - b^n$ Eliminate \mathbf{u} $F_2(\mathbf{u}) = \mathbf{v} - \Psi((M + \Delta L)^{-1}(b - M\mathbf{v}))$

Jacobian for coupled formulation, with $D = \text{diag}(\Psi'(\boldsymbol{u}_1), \dots, \Psi'(\boldsymbol{u}_N))$

$$J = \begin{pmatrix} M + \Delta L & M \\ -D & I \end{pmatrix}$$

 $J_2 = I + D(M + \Delta tL)^{-1}M$ is Schur complement of J

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- Solve the linear system by an iterative method (GMRES)
- Requires only jacobian matrix by vector products.

Used for CFD, shallow water, radiative transfer(Keyes, Knoll, JCP 04), and for reactive transport (Hammond et al., Adv. Wat. Res. 05)



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Inexact Newton

- Approximation of the Newton's direction $||f'(x_k)d + f(x_k)|| \le \eta ||f(x_k)||$
- Choice of the forcing term η?
 - Keep quadratic convergence (locally)
 - Avoid oversolving the linear system

• $\eta = \gamma \|f(x_k)\|^2 / \|f(x_{k-1})\|^2$ (Kelley, Eisenstat and Walker)

- Essential for good linear performance
- Difficult for matrix free formulation

Possible choices

Block diagonal $P = \text{diag}(M + \Delta tL, I)$,

Block Gauss Seidel "Physics based", equivalent to (lienar) sequential method

$$P = \begin{pmatrix} M + \Delta t L & 0 \\ -D & I \end{pmatrix}$$

Aproximate block factorization ?

Geometry of MoMaS reactive transport benchmark (2D), LifeV + Kinsol (Sundials)

σ_0	0.125	0.25	0.4	0.45	0.5
nb nonlin iter	5	6	6	6	7
nb lin. iter	12	19	27	43	86



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Transport for each species (same dispersion tensor for all species) Eliminate (unknown) reaction rates by using conservation laws (T = C + F)

$$\begin{split} \omega \frac{\partial T^{ic}}{\partial t} + \mathcal{L}(C^{ic}) &= 0, \quad ic = 1, \dots, N_c \\ T^{ic}_{ix} &= C^{ic}_{ix} + F^{ic}_{ix} \qquad ic = 1, \dots, N_c \text{ and } ix = 1, \dots, N_x \\ F_{ix} &= \Psi(T_{ix}) \qquad ix = 1, \dots, N_x. \end{split}$$

Coupling methods

Iterative, based on fixed point (Yeh Tripathi '89, Carrayrou et al. '04) Substitution, global (Saaltink '98, Hammond et al. '05) Reduction method (Knabner, Kratle, '06)

CC formulation, explicit chemistry

$$\begin{cases} \omega \frac{dC}{dt} + \frac{dF}{dt} + LC = 0 \\ H(z) - \binom{C+F}{W} = 0 \\ F - F(z) = 0. \end{cases}$$

• + Explicit Jacobian

- + Chemistry function, no chemical solve
- Intrusive approach (chemistry not a black box)
- - Precipitation not easy to include

Coupled system is index 1 DAE

$$K\frac{dy}{dt}+f(y)=0$$

Use standard DAE software

C. de Dieuleveult (Andra thesis), J. Erhel, MK (JCP '09)

TC formulation, implicit chemistry

$$\begin{cases} \omega \frac{dT}{dt} + LC = 0\\ T - C - F = 0\\ F - \Psi(T) = 0 \end{cases}$$

- + Non-intrusive approach (chemistry as black box)
- + Precipitation can (probably) be included
- One chemical solve for each function evaluation

$$\begin{cases} C^{n+1} = (M + \Delta tL)^{-1} (C^{n} + F^{n} - F^{n+1}) \\ T^{n+1} = C^{n+1} + F^{n+1} \\ F^{n+1} = \Psi(T^{n+1}) \end{cases}$$

Fixed point problem, can be solved by block Gauss Seidel or by Newton's method

Solution by Newton–Krylov

Structure of Jacobian matrix

$$f'(C, T, F) = \begin{pmatrix} I & 0 & (I + \Delta tL)^{-1} \\ -I & I & -I \\ 0 & -\Psi'(T) & I \end{pmatrix}$$



- Transport independant for each species
- Chemistry independant for each grid cell

Find a good preconditioner ?

- Is block diagonal good enough ?
- Physics based (cf Hammond et al.) ?

Example: ion exchange

Column experiment (Phreeqc ex. 11, Alliances ex. 3)



Column contains a solution with 1mmol Na, 0.2mmol K and 1.2mmol NO₃. Inject solution with 1.2mmolCaCl₂. $CEC = 1.110^{-3}$.



Ion exchange example (ctd)

Snapshots at t = 35







Na



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Difficult test case, heterogenous medium, with complex chemistry (even for "easy" level).

12 species, eq. constants vary by 45 orders of magnitude (1D, Matalb code, L.Amir's thesis).



- Robust methods for solving flow and transport in porous media
- Preliminary results for reactive transport
- Newton–Krylov promising framework, implementation in progress
- Move to two-phase (multiphase) flows (water and gas)
- Transport in fractured media
- For chemistry, take into account "real" phenomena (minerals, kinetics,...)